

Detection of Hydroxylamine Intermediate Opens a New Perspective on Ammonia Selectivity in Metal-Catalyzed Nitrate Reduction

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Significance and Relevance

In the catalytic reduction of nitrates in drinking water, undesired NH_4^+ formation is the main drawback yet hindering this technology from industrial application. Despite that most studies claim nitrites (NO_2^-), ammonium cations (NH_4^+), and nitrogen (N_2) as the exclusive reaction products, we found hydroxylamine (NH_2OH) as additional product under typical NO_3^- reduction conditions (~pH 6). We observed the degradation of NH_2OH into NH_4^+ over time suggesting that NH_2OH may be formed in typical NO_3^- reduction systems, but might be overseen if not specifically searched for. This observation questions not only NH_4^+ selectivity in existing studies, but also gives a new perspective on the underlaying reaction mechanism of the catalytic NO_3^- reduction.

Introduction and Motivations

In the European Union around 14 % of the groundwater stations exceeded the NO₃⁻ limit of 50 mg/L, and about one third of the land waters and more than 80 % of the ocean waters in the EU are considered eutrophic, showing the demand for improved NO₃⁻ management.^[1] Catalytic NO₃⁻ reduction is a potential technology to remove NO₃⁻ from water bodies by actually degrading it into harmless N₂, which makes it in this aspect superior to alternative techniques such as reverse osmosis, ion exchange or electrodialysis as no concentrated waste brines are generated.^[2] Bimetallic Pd-Cu, Pd-Sn and Pd-In catalysts actively reduce NO₃⁻ in the presence of H₂ at RT and atmospheric pressure while the major challenge is the undesired NH₄⁺ production as e.g. the limits in drinking water are even stricter than for NO₃⁻ (0.5 mg/L vs. 50 mg/L).^[2]

The standard procedure in scientific literature is to determine NH_4^+ , NO_2^- and NO_3^- concentrations by IC or HPLC, assuming that the remainder is N_2 . Closing the N mass balance entirely is extremely challenging as gas and liquid phase samples exhibit a delay but must be matched. Additionally, contamination with atmospheric N_2 is difficult to suppress. Only few studies achieve a closed mass balance over parts of the reaction time,^[4] or during the entire reaction only by using isotope labeled $N.^{[3]}$ In this study, we show an easy method to detect NH_2OH in NO_3^- reduction as it is easily overseen if not carefully checked for.

Materials and Methods

A Pd/Al₂O₃ catalyst (2.5 wt% Pd, 181 m²/g, < 45 μ m) was prepared via Strong Electrostatic Adsorption method ([Pd(NH₄)₄](NO₃)₂ and NH_{3,aq}). From this, a bimetallic SnPd/Al₂O₃ (Pd : Sn ratio 1.4 : 1) catalyst was prepared via sequential impregnation (SnCl₂ in ethanol). The catalysts were characterized by XRF, CO-chemisorption, N₂-physisorption, XRD and TEM. NO₃⁻ and NO₂⁻ (1 mM) were converted in a 1 L semi-batch reactor under continuous gas flow (H₂, CO₂, He) in the absence of mass transport limitations. Liquid samples were taken over time and benzaldehyde or acetone were added to derivatize NH₂OH into the corresponding oxime. NO₃⁻, NO₂⁻ and NH₄⁺ were quantified by ion chromatography and the oxime by HPLC or GC after derivatization.

Results and Discussion

In a conventional NO₃⁻ reduction experiment over a SnPd/Al₂O₃ catalyst, NO₂⁻ is only observed in traces ($\leq 0.01 \text{ mM}$) and the NH₄⁺ concentration increases with increasing NO₃⁻ conversion but plateaus after full NO₃⁻ depletion. However, we observed increasing NH₄⁺ concentrations even after full NO₃⁻



conversion. Therein, the NH_4^+ concentration increase was larger than the accessible moles of metal surface and could thus not be explained by desorption of surface N-species suggesting an additional reaction intermediate, which could be defined as NH_2OH by it trapping into an oxime with benzaldehyde or acetone (Figure 1 **B**).



Time / min

Figure 1: A Concentration profile of NO_3^- reduction reaction. Reaction conditions: 1 mM KNO₃, 50 mg SnPd/Al₂O₃, 80:10:10 mL/min H₂:CO₂:He, RT, 300 mL milli-Q water, 600 rpm. **B** Schematic reaction pathway of NH₂OH trapping into an oxime or decomposition into NH₄⁺.

The typical concentration profile in Figure 1 **A** shows an initially strong NH₂OH formation resulting in a maximum NH₂OH selectivity of 47 %. Over time, NH₂OH decomposes mainly into NH₄⁺, but as the sum of NH₂OH and NH₄⁺ concentration decreases, also partly into N₂. The NH₂OH decomposition occurs also after catalyst removal and is thus non-catalytic. Experiments to elucidate whether the decomposition follows a hydrogenation or disproportionation are ongoing.

The addition of hydroxylamine scavenger in the reactor does not entirely suppress the NH_4^+ formation indicating that probably not all NH_4^+ is formed via the NH_2OH pathway or, less likely, the difference in oxime formation rate and NH_2OH decomposition rate is insufficiently large to trap all NH_2OH . These research questions are currently under investigation in our group also for the NO_2^- reduction on SnPd/Al₂O₃ and Pd/Al₂O₃ catalysts.

This study suggests that NH₂OH is possibly a key reaction intermediate in the NO₃⁻ reduction reaction over a SnPd/Al₂O₃ catalyst. Trapping this NH₂OH using acetone or benzaldehyde into an oxime offers a simple and transferrable quantification strategy, which can substantially improve our understanding of this reaction. The detection of NH₂OH as reaction intermediate should encourage to critically question reported NH₄⁺ selectivity and more broadly the reaction mechanism behind NH₄⁺ and N₂ formation.

References

- 1. European Commission, <u>Report on the implementation of Council Directive 91/676/EES concerning</u> the protection of waters against pollution caused by nitrates [...] **2021**.
- 2. I. Sanchis, E. Diaz, A.H. Pizarro, J.J. Rodriguez, A.F. Mohedano, *Sep. Purif. Technol.* **2022**, 290, 120750.
- 3. R. Zhang, D. Shuai, K. A. Guy, J.R. Shapley, T.J. Strathmann, C.J. Werth, ChemCatChem **2013**, 5, 313-321.
- 4. U. Prüsse, J. Daum, C. Bock, K.-D. Vorlop, Stud. Surf. Sci. 2000, 130, 2237-2242.

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