

Uniform SiO₂@CeO₂ core-shell structures doped with CuO and Co₃O₄ as efficient catalysts for toluene combustion

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Significance and Relevance

Finding optimal catalysts for the total oxidation of volatile organic compounds (VOCs) is currently a significant challenge due to an increasing level of air pollution and threats related to the VOCs emission. Oxide systems can be successfully used in this process but they have to be optimally designed in terms of composition and distribution of both active phase and support. The presented work shows the potential of materials based on the synergy between the CuO, Co_3O_4 and CeO_2 phases arranged in one catalytic bed working in the toluene combustion.

Preferred and 2nd choice for the topic: Air cleaning and combustion, Automotive and stationary emission control (2nd choice)

Preferred presentation: Oral preferred or Short Oral

Introduction and Motivations

One of the most important challenges for environmental sustainability is to reduce the emission of harmful VOCs into the atmosphere. In light of the constantly tightening regulations, many technologies for effective removal of VOCs have been developed, including catalytic total oxidation over materials containing noble metals (e.g. Pt, Pd, Au, Ag) and transition metal oxides (e.g. CuO, MnO₂, Fe₂O₃, Co₃O₄). The transition metal oxide catalysts, despite their lower activity compared to noble metals, are much cheaper and more resistant to poisoning.¹ On the other hand, their lower catalytic activity can be partially compensated by a proper design of active phase support. For example, cerium(IV) oxide can be effectively used in this role. CeO₂ has attractive properties due to a large number of oxygen defects that favor an extraordinary capacity for storing and releasing oxygen. Furthermore, CeO₂ provides enhanced thermal stability and high dispersion of the active phase. Although ceria can act as a singlecomponent catalyst in the VOCs combustion, its activity can be significantly improved by an introduction of transition metal oxides. In such a case, a synergistic effect appears due to the formation of redox pairs Ce^{4+}/Ce^{3+} and $Me^{n+}/Me^{(n-1)+}$ leading to enhanced oxygen mobility. In the presented work, CuO/CeO_2 and Co_3O_4/CeO_2 oxide systems were deposited on nanometric, non-porous SiO₂ spheres to form novel core-shell SiO₂@CeO₂/MeO_x (Me = Cu or Co) catalysts. Such a catalyst grain design allowed for better exposure of the active components of the material to the reaction mixture.² The catalytic performance of individual and variously mixed systems in the combustion of toluene, as a representative of aromatic VOCs, was discussed.

Materials and Methods

SiO₂ spheres were prepared using the Stöber strategy. To facilitate the deposition of a precursor of another oxide phase on the SiO₂ surface, it was initially modified by anchoring an aminosilane coupling agent, i.e. 3-aminopropyltriethoxysilane (APTES). A core-shell SiO₂@CeO₂ support structure was synthesized by precipitation of a CeO₂ precursor on the surface of a spherical silica scaffold at constant pH. Finally, the formed SiO₂@CeO₂ support was modified with transition metal oxide precursors using the wet impregnation method to obtain the Co or Cu content of 5, 10, and 15 wt.% in the final catalysts.

Extensive physicochemical characterization was performed for the synthesized catalysts in terms of their morphology (SEM-EDS), surface and bulk composition (XPS and XRF), textural parameters (N_2 adsorption), structure (XRD), chemical environment (UV-Vis-DR), and reducibility (H_2 -TPR). Most importantly, the catalytic performance of the developed materials in the combustion of toluene was studied.



Results and Discussion

The SEM images of the SiO₂@CeO₂ support revealed the homogeneous distribution of the CeO₂ phase, allowing the formation of the uniform shell while minimizing the presence of small bulk CeO₂ aggregates in interparticle voids. Conversely, the materials after Co and Cu oxide deposition showed slight particle aggregation due to the formation of clusters of active phase species on the support surfaces. However, a consistent spherical shape with a smooth surface was maintained. The deposition of CeO₂ significantly altered mesoporosity of the material. Nevertheless, the subsequent introduction of the active phase affected porosity due to its penetration into the pores formed by the CeO₂ washcoat. The formation of CeO₂, CuO, and Co₃O₄ phases for both the support revealed an absorption band associated with electron transitions in CeO₂. The Co-containing catalysts exhibited two additional wide bands, indicating the presence of Co₃O₄ phase. Furthermore, all copper catalysts displayed a low intense band below 300 nm attributed to the charge transfer O²⁻ \rightarrow Cu²⁺, validating the existence of small crystalline CuO particles.

The critical aspect of the study was evaluating the activity of the obtained $SiO_2@CeO_2/MeO_x$ coreshell materials in total oxidation of toluene (Figure 1). It was proven that the introduction of CuO significantly lowers the initial temperature of the toluene conversion, while Co_3O_4 promotes superior catalytic performance at higher temperatures. Various arrangements of the bicomponent catalytic bed (containing both $SiO_2@CeO_2/CuO$ and $SiO_2@CeO_2/Co_3O_4$ materials) were tested to ensure operation over a wide range of temperatures. The catalyst composition was mixed in two ways: (i) the Cu and Co-containing catalysts were homogenously mixed at various ratios, or (ii) the catalysts were arranged in layers.

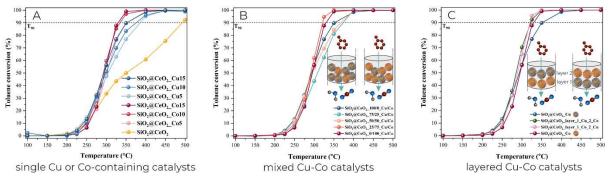


Figure 1. Catalytic activity in the toluene combustion of (A) single Co and Cu-containing, as well as (B) mixed Co-Cu and (C) layered Co-Cu catalysts.

The catalytic results confirm that the catalyst composition, including metal molar ratios, significantly influence the activity in the toluene combustion. The co-performance of the catalysts containing CuO and Co_3O_4 phases exhibits interesting correlations at their direct contact and separation. Furthermore, the stability tests of the developed catalysts in the toluene combustion were carried out at a specific temperature. The catalytic performance was tested alternatively in dry (1000 ppm of toluene in 100 ml/min of air) or wet atmosphere (1000 ppm of toluene in 100 ml/min of air saturated with 10 % vol. of H₂O). The developed systems demonstrated high stability, maintaining a high level of toluene conversion during 24 h measurements.

References

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